

# OPTIMISING DESLIMING CIRCUITS WITH CLASSIFYING CYCLONES

SACPS Coal Metallurgists & Plant Operators Workshop Frikkie Enslin – MPE Applications Manager 21 September 2022

#### Disclaimer!

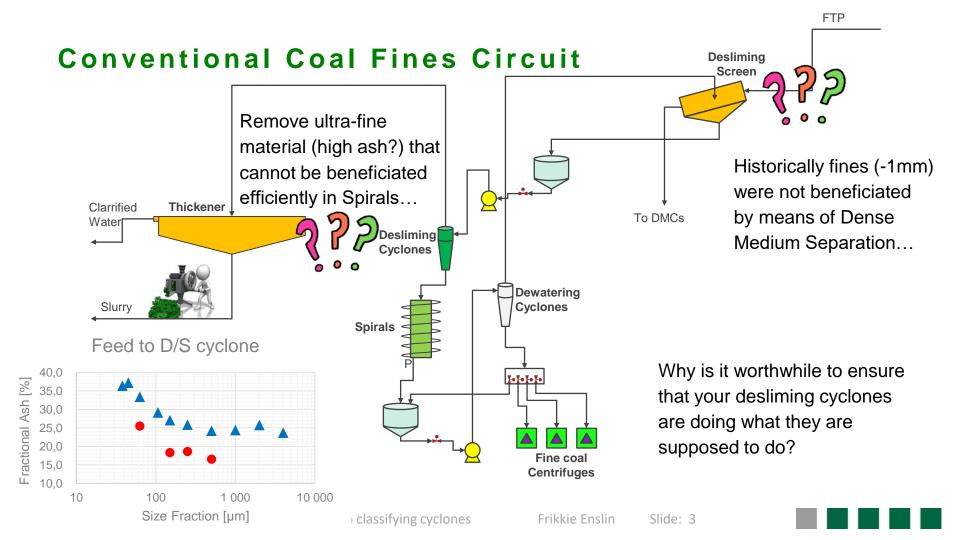
L – Excessive use of the F-word… "Fines"

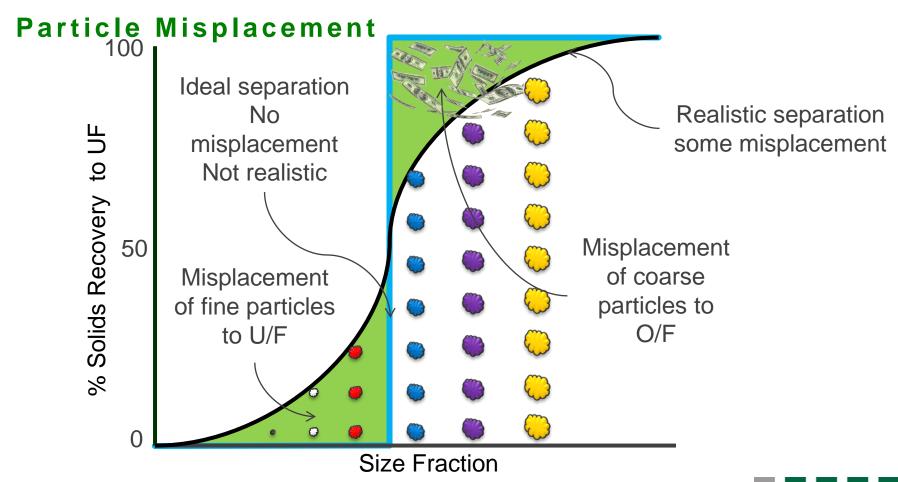
V – Value adding tips and tricks



N – New / renewed focus on a brilliant piece of technology

S – Fortunately no selling today, only sharing





#### What can be done?

How do we reduce the potential revenue we're discarding in our desliming cyclones' overflow?

- Reduce the desliming cyclone cut point
- Minimise misplacement of coarse particles to the overflow
- Preventative maintenance and best operational practices
- New / fresh thinking around the fines circuit

The first prize will be to get the best out of whatever is already on site.









## Reduce desliming cyclone cutpoint

Reducing the desliming cyclone cut point = minimise loss of coarse material to the overflow.

The following options are available to achieve this without installing smaller diameter units:

- Installing larger spigot diameters  $\rightarrow$  Increased  $\theta$  (including fines!)
- Installing smaller vortex finders → Finer cutpoint & reduced cyclone capacity
- Reduction of cyclone feed solids concentration → Better efficiencies, pumps?



Make sure you understand the impact these changes will have on:

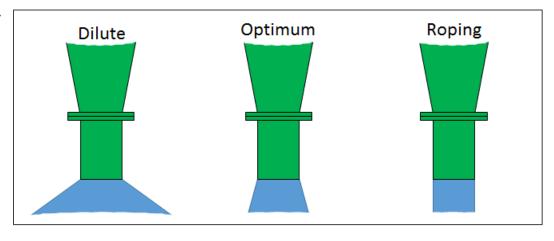
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- Spiral plant capacity
- Dewatering cyclones
- Thickener & Filter press

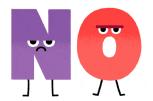
- Feed pressure
  - Main causes for fluctuations in feed pressure:
    - Incorrect feed sump design (solids shouldn't be slumping on the sides of the sump)
    - The sump's level control may be faulty
    - There may be fluctuating feed into the sump
  - Too high accelerated wear
  - Too low air core instability
- Spigot discharge profile
- Overflow siphoning

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- Cyclone carries the weight of the feed pipe
- Weight pulls the alignment of cyclone internals skew
- Bend in the feed close to the cyclone's inlet
- Surging pump



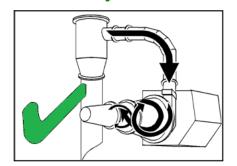


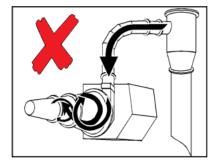
- The weight of the feed pipe should be supported by infrastructure
- Feed pipe should be straight for at least 9 pipe diameters
- Constant feed conditions

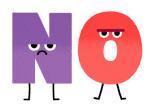




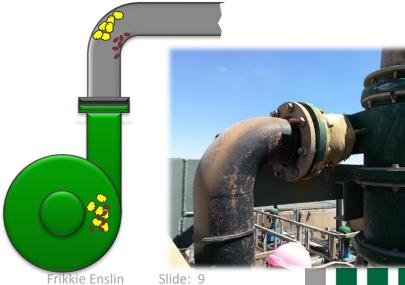






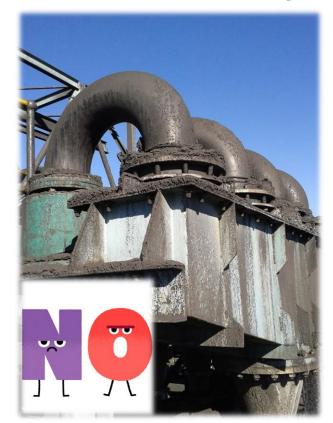






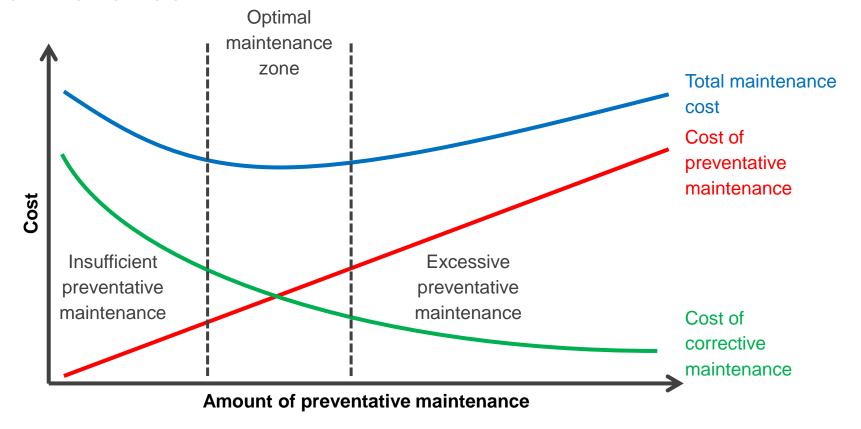
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Optimising desliming circuits with classifying cyclones





#### Maintenance



Slide: 11

#### Maintenance

Allowed spigot wear – 10%

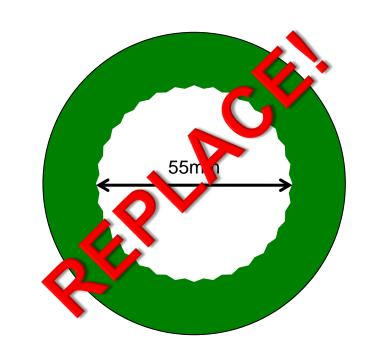
Original spigot size: 50mm

Allowed wear: 10% x 50mm

=5mm

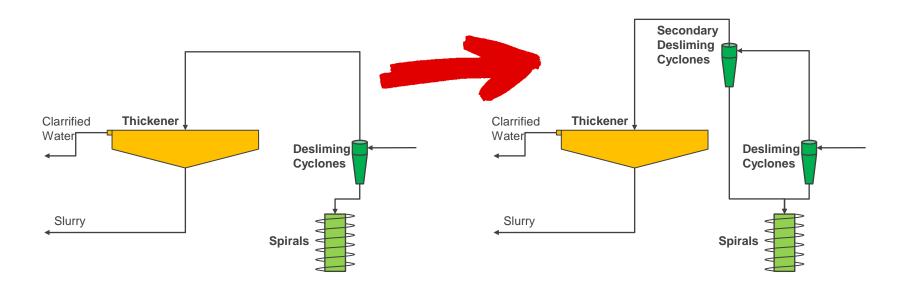
Change size: 50mm + 5mm

= 55mm



## New / fresh thinking around the fines circuit

What if we attempt to recover the misplaced particles in the desliming cyclone's overflow with a secondary / scavenger cyclone?



## New / fresh thinking around the fines circuit

#### **Particle Size Distribution:**

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Size	Cumulative % Passing		
Microns	Feed	Underflow	Overflow
3000	100.0	100.0	100.0
1000	100.0	100.0	100.0
500	56.4	46.3	100.0
212	39.0	24.9	100.0
150	36.4	22.0	98.9





$$= 100 - 98.9 = 1.1\%$$

$$9.4$$
tph x  $1.1\% = 0.1$ tph

94% is < 15% Ash

 $\rightarrow$  94% x 0.1tph

= 0.09tph potential export product

@ R4,400 per ton (May'22)

≈ R400/hr potential revenue



50tph





## Final thought

Cyclones (whether DMS or hydrocyclones) are at the heart of our conventional coal processing plants.

If you take care of them, they will return the favour.

If you don't know or are unsure how to take care of your plant's heart...

Make an appointment with the doctors!

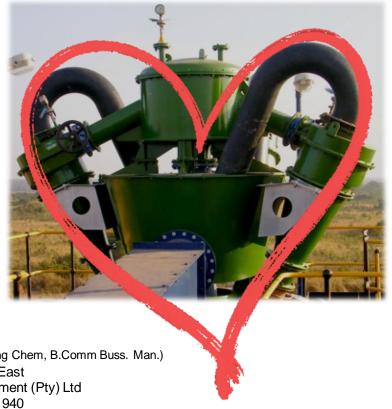
Wink, wink, nudge, nudge



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